

# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## INTRODUCTION

In the engineering of thermoplastic piping systems, it is necessary to have not only a working knowledge of piping design but also an awareness of a number of the unique properties of thermoplastics.

In addition to chemical resistance, important factors to be considered in designing piping systems employing thermoplastics are:

1. Pressure ratings.
2. Water hammer.
3. Temperature-Pressure relationships.
4. Friction-loss characteristics.
5. Dimensional and Weight data.

These factors are considered in detail in this section.

## PRESSURE RATINGS OF THERMOPLASTICS

### DETERMINING PRESSURE-STRESS-PIPE RELATIONSHIPS

#### ISO EQUATION

Circumferential stress is the largest stress present in any pressurized piping system. It is this factor that determines the pressure that a section of pipe can withstand. The relation-ship of stress, pressure and pipe dimensions is described by the ISO (for International Standardization Organization) Equation. In various forms this equation is:

$$P = \frac{2S}{R-1} = \frac{2St}{D_o-t} \quad \frac{2S}{P} = \left(\frac{D_o}{t}\right) - 1$$

$$\frac{2S}{P} = R - 1 \quad S = \frac{P(R-1)}{2}$$

Where:

- P = Internal Pressure, psi
- S = Circumferential Stress, psi
- t = Wall thickness, in.
- D<sub>o</sub> = Outside Pipe diameter, in.
- R = D<sub>o</sub>/t

### LONG-TERM STRENGTH

To determine the long-term strength of thermoplastic pipe, lengths of pipe are capped at both ends (see Figure 1) and subjected to various internal pressures, to produce circumferential stresses that will produce failure in from 10 to 10,000 hours. The test is run according to ASTM D 1598 — Standard Test for Time-to-Failure of Plastic Pipe Under Long-Term Hydrostatic Pressure.

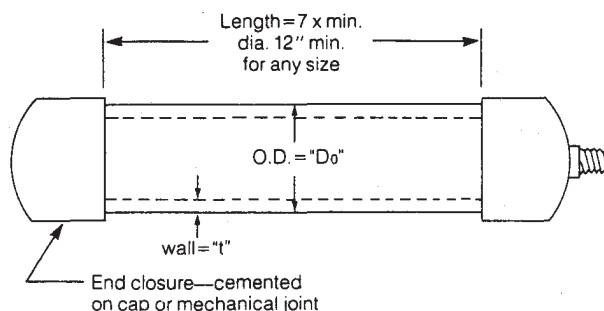
The resulting failure points are used in a statistical analysis (outlined in ASTM D-2837; see page 6 to determine the characteristic regression curve that represents the stress/time-to-failure relationship for the particular thermoplastic pipe compound under test. This curve is represented by the equation:  $\text{Log} = a + b \text{Log } S$

Where:

a and b are constants describing the slope and intercept of the curve, and T and S are time-to-failure and stress, respectively.

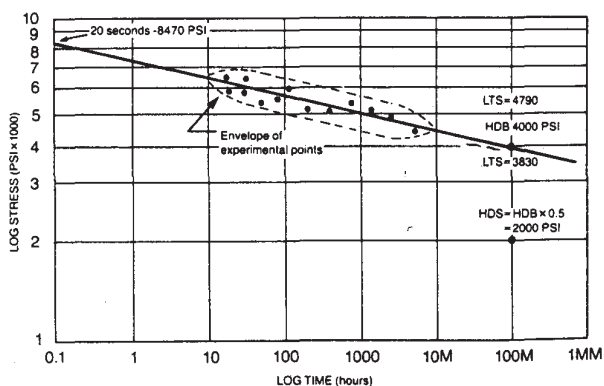
The regression curve may be plotted on a log-log paper, as shown in Figure 2, and extrapolated from 10,000 to 100,000 hours (11.4 years). The stress at 100,000 hours is known as the Long Term Hydrostatic Strength (LTHS) for that particular thermoplastic compound. From this (LTHS) the Hydrostatic Design Stress (HDS) is determined by applying the service factor multiplier, as described below.

**FIGURE 1**  
LONG-TERM STRENGTH TEST PER ASTM D1 598



Pipe test specimen per ASTM D 1598 for "Time-to-Failure of Plastic Pipe Under Long-Term Hydrostatic Pressure"

**FIGURE 2**  
REGRESSION CURVE—STRESS/TIME-TO-FAILURE FOR PVC TYPE I



### SERVICE FACTOR

The Plastics Pipe Institute (PPI) has determined that a service (design) factor of one-half the Hydrostatic Design Basis would provide an adequate safety margin for use with water to ensure useful plastic-pipe service for a long period of time. While not stated in the standards, it is generally understood within the industry that this "long period of time" is minimum of 50 years.

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Accordingly, the standards for plastic pipe, using the 0.5 service factor, required that the pressure rating of the pipe be based upon this Hydrostatic Design Stress, again calculated with the ISO equation.

While early experience indicated that this service factor, or multiplier, of 0.5 provided adequate safety for many if not most uses, some experts felt that a more conservative service factor of 0.4 would better compensate for water hammer pressure surges, as well as for slight manufacturing variations and damage suffered during installation.

The PPI has issued a policy statement officially recommending this 0.4 service factor. This is equivalent to recommending that the pressure rating of the pipe should equal 1.25 times the system design pressure for any particular installation. Based upon this policy, many thousands of miles of thermoplastic pipe have been installed in the United States without failure.

It is best to consider the actual surge conditions, as outlined later in this section. In addition, substantial reductions in working pressure are advisable when handling aggressive chemical solutions and in high-temperature service.

Numerical relationships for service factors and design stresses of PVC are shown in Table I-A below.

## SERVICE FACTORS AND HYDROSTATIC DESIGN STRESS (HDS)\*

SERVICE FACTOR	HDS
0.5	2000 psi (13.8 MPa)
0.4	1600 psi (11 MPa)

\*Material: PVC Type 1 & CPVC

## TEMPERATURE-PRESSURE AND MODULUS RELATIONSHIPS

### Temperature Derating.

Pressure ratings for thermoplastic pipe are generally determined in a water medium at room temperature (73°F). As the system temperature increases, the thermoplastic pipe becomes more ductile, increases in impact strength and decreases in tensile strength. The pressure ratings of thermoplastic pipe must therefore be decreased accordingly.

The effects of temperature have been exhaustively studied and correction (derating) factors developed for each thermoplastic piping compound. To determine the maximum operating pressure at any given temperature, multiply the pressure rating at ambient shown in Table 1 by the temperature correction factor for that material shown in Table 2. Attention must also be given to the pressure rating of the joining technique i.e. Threaded system normally reduces pressure capabilities, substantially.

**TABLE 1**

### MAXIMUM OPERATING PRESSURES (PSI) AT 73°F AMBIENT BASED UPON A SERVICE FACTOR OF .5

NOMINAL SIZE	PVC & CPVC SCHEDULE 40 SOLVENT WELD	PVC & CPVC SCHEDULE 80		POLYPROPYLENE*(PP)			POLYVINYLIDENE FLUORIDE (PVDF)				
		SOLVENT WELD	THREADED	PPRO-SEAL	PROLINE SDR		SUPER PROLINE SDR		SCHEDULE 80		
					11	32	11	32	SOCKET FUSION	THREADED	
1/4	780	1130	---	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
3/8	620	920	---	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
1/2	600	850	420	150	160	45	230	N/A	975	290	
3/4	480	690	340	150	160	45	230	N/A	790	235	
1	450	630	320	150	160	45	230	N/A	725	215	
1-1/4	370	520	260	N/A	160	45	230	N/A	600	180	
1-1/2	330	471	240	150	160	45	230	N/A	540	160	
2	280	400	200	150	160	45	230	N/A	485	135	
2-1/2	300	425	210**	N/A	160	45	N/A	160	N/A	N/R	
3	260	375	190**	N/A	160	45	N/A	160	430	N/R	
4	220	324	160**	N/A	160	45	N/A	160	370	N/R	
6	180	260	N/R	N/A	160	45	N/A	160	N/A	N/R	
8	160	250	N/R	N/A	160	45	N/A	160	N/A	N/A	
10	140	230	N/R	N/A	160	45	N/A	160	N/A	N/A	
12	130	230	N/R	N/A	160	45	N/A	160	N/A	N/A	

--- = Data not available at printing; N/R = Not Recommended; N/A = Not Available (not manufactured)

\* Threaded Polypropylene is not recommended for pressure applications and Fusual drainage systems are not pressure rated.

\*\*For threaded joints properly backwelded.

NOTE: The pressure ratings in this chart are based on water and are for pipe and fittings only. Systems that include valves, flanges, or other weaker items will require derating the entire system.

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**Table 2**  
**TEMPERATURE CORRECTION FACTORS**

OPERATING TEMPERATURES °F	FACTORS					
	PVC	CPVC	POLYPROPYLENE		POLYVINYLIDENE FLUORIDE	
			PPRO-SEAL NATURAL	PROLINE	SUPER PROLINE	SCHEDULE 80
73	1.00	1.00	1.00	1.00	1.00	1.00
80	.88	.94	.93		.95	.93
90	.75	.86	.83		.87	.87
100	.62	.78	.74	.64	.80	.82
110	.50	.71	.66			.76
120	.40	.64	.58		.68	.71
130	.30	.57	.51			.65
140	.22	.50	.40	.40	.58	.61
150	N/R	.43	.38			.57
160	N/R	.37	.35		.49	.54
180	N/R	.25	.23	.28	.42	.47
200	N/R	.18	.14	.10	.36	.41
210	N/R	.16	.10	N/R		.38
220	N/R	N/R	N/R	N/R		.35
240	N/R	N/R	N/R	N/R	.25	
250	N/R	N/R	N/R	N/R		.28
280	N/R	N/R	N/R	N/R	.18	.22

## FLANGED SYSTEMS

**Table 3 - MAXIMUM OPERATING PRESSURE (PSI) FOR FLANGED SYSTEMS**

OPERATING TEMPERATURE °F	PVC*	CPVC*	PP**	PVDF
100	150	150	150	150
110	135	145	140	150
120	110	135	130	150
130	75	125	118	150
140	50	110	105	150
150	N/R	100	93	140
160	N/R	90	80	133
170	N/R	80	70	125
180	N/R	70	50	115
190	N/R	60	N/R	106
200	N/R	50	N/R	97
210	N/R	40	N/R	90
240	N/R	N/R	N/R	80
280	N/R	N/R	N/R	25

N/R = Not Recommended

\* PVC and CPVC flanges sizes 2-1/2 through 3- and 4-inch threaded must be backwelded for the above pressure capability to be applicable.

\*\* Threaded PP flanges size 1/2 through 4 inch as well as the 6" back welded socket flange are not recommended for pressure applications (drainage only).

### FLANGED SYSTEMS

Maximum pressure for any flanged system is 150 psi. At elevated temperatures the pressure capability of a flanged system must be derated as shown in Table 12.

Design Pressure - Pressure rating at 73°F x temperature correction factor.

# PRESSURE RATINGS

## PVC LARGE DIAMETER FABRICATED FITTINGS

### AT 73°F 10" THROUGH 24"

The following tables indicate the working pressure recommended by the manufacturer for large diameter PVC fabricated fittings. These fittings are not generally recommended for high pressure applications. Pressure capabilities are not necessarily the same as the rating of the pipe from which they are fabricated. Be sure pressure to temperature correction factors are considered when system design calls for temperatures above 73°F.

Water hammer and surge pressure are the two most critical elements in large-diameter design. Keeping velocities below 5 feet per second and working pressures to these guidelines will give years of trouble-free service.

**Table 4**  
**90° ELBOW**

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	22	140	34	230
12	30	130	50	230
14	40	130	70	220
16	56	130	100	220
18	90	100	93	125
20	121	50	125	75
24	202	50	208	75

**Table 7**  
**45° ELBOW**

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	15	140	24	230
12	21	130	36	230
14	30	130	52	220
16	42	130	75	220
18	47	100	71	160
20	62	50	95	75
24	103	50	159	75

**Table 5**  
**COUPLING**

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	9	140	15	230
12	15	130	23	230
14	19	130	33	220
16	29	130	54	220
18	33	100	53	160
20	45	50	74	75
24	77	50	110	75

**Table 8**  
**REDUCING TEE**

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10 x 8	23	140	32	230
10 x 6	21	140	30	230
10 x 4	18	140	28	230
12 x 10	32	130	55	220
12 x 8	30	130	49	220
12 x 6	26	130	47	220
12 x 4	24	130	45	220
14 x 12	46	100	70	160
14 x 10	39	100	66	160
14 x 8	36	100	59	160
16 x 14	68	100	118	160
16 x 12	61	100	105	160
16 x 10	54	100	90	160
16 x 8	49	100	82	160
18 x 16	82	100	132	160
18 x 14	73	100	116	160
20 x 18	104	75	160	100
20 x 16	98	75	156	100
24 x 20	162	50	251	75

**Table 6**  
**TEE**

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	28	140	44	230
12	41	130	69	230
14	54	130	95	220
16	78	130	139	220
18	115	100	156	160
20	153	50	204	75
24	231	50	338	75

# PRESSURE RATINGS

## PVC LARGE DIAMETER FABRICATED FITTINGS

### AT 73°F 10" THROUGH 24"

**Table 9**  
CONCENTRIC REDUCER

NOMINAL SIZE (IN.)	SCHEDULE 40	
	WT. (LBS.)	PSI RTG
10 x 8	9	140
10 x 6	22	140
10 x 4	23	140
12 x 10	15	130
12 x 8	31	130
12 x 6	34	130
14 x 12	23	130
14 x 10	36	130
16 x 14	32	130
16 x 12	54	130
18 x 16	48	100
20 x 18	45	100
24 x 20	87	100

**Table 10**  
BUSHING (SPIG x SOC)

NOMINAL SIZE (IN.)	SCHEDULE 40	
	WT. (LBS.)	PSI RTG
10 x 8	11	140
10 x 6	16	140
10 x 4	20	140
12 x 10	15	130
12 x 8	26	130
12 x 6	31	130
14 x 12	24	100
16 x 14	22	100
16 x 12	46	100
16 x 10	61	100
16 x 8	72	100
18 x 16	30	100
20 x 18	33	100
24 x 20	55	100

**Table 11**  
EXTENDED BUSHING

NOMINAL SIZE (IN.)	SCHEDULE 40	
	WT. (LBS.)	PSI RTG
10 x 8	11	140
12 x 10	19	130
14 x 12	28	130
16 x 14	38	130

**Table 12**  
MALE ADAPTOR

NOMINAL SIZE (IN.)	SCHEDULE 40	
	WT. (LBS.)	PSI RTG
6	6	25
8	7	25
10	8	25
12	14	25

**Table 13**  
FEMALE ADAPTOR

NOMINAL SIZE (IN.)	SCHEDULE 40	
	WT. (LBS.)	PSI RTG
6	6	25
8	7	25
10	8	25
12	14	25

# PRESSURE RATINGS

## PVC LARGE DIAMETER FABRICATED FITTINGS

### AT 73°F

**Table 14**  
CROSS

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
3	2	240	5	260
4	3	220	7	240
6	13	160	22	240
8	22	160	30	240
10	38	140	62	230
12	58	130	95	230
14	74	130	129	220
16	107	130	190	220
18	117	100	185	160
20	158	50	247	75
24	267	50	413	75

**Table 15**  
FLANGE (BLIND)

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	16	25	32	75
12	21	25	42	75
14	26	25	52	75
16	33	25	66	75
18	36	25	72	75
20	44	25	88	75
24	57	25	114	75

**Table 16**  
CAP

NOMINAL SIZE (IN.)	SCHEDULE 40		SCHEDULE 80	
	WT. (LBS.)	PSI RTG	WT. (LBS.)	PSI RTG
10	5	140	14	230
12	7	130	17	230
14	23	130	35	220
16	32	130	49	220
18	38	100	54	160
20	49	50	69	75
24	74	50	108	75

**Table 17**

IPS PIPE DIMENSION TABLE

NOMINAL PIPE SIZE (IN.)	O.D.	SCHEDULE 40		SCHEDULE 80	
		AVERAGE I.D.	MINIMUM WALL	AVERAGE I.D.	MINIMUM WALL
1	1.315	1.033	.133	.935	.179
1-1/4	1.660	1.364	.140	1.256	.191
1-1/2	1.900	1.592	.145	1.476	.200
2	2.375	2.049	.154	1.913	.218
3	3.500	3.042	.216	2.864	.300
4	4.500	3.998	.237	3.786	.337
5	5.563	5.047	.258	4.813	.375
6	6.625	6.013	.280	5.709	.432
8	8.625	7.943	.322	7.565	.500
10	10.750	9.976	.365	9.492	.593
12	12.750	11.890	.406	11.294	.687
14	14.000	13.126	.437	12.440	.780
16	16.000	15.000	.500	14.200	.900
		CLASS 100		CLASS 160	
18	18.000	17.120	.440	16.614	.693
20	20.000	19.022	.489	18.460	.770
24	24.000	22.870	.585	22.152	.924

# SYSTEMS ENGINEERING DATA

## FOR THERMOPLASTIC PIPING

**Table 18**

**MODULUS OF ELASTICITY (x10<sup>10</sup>) PSI VS. TEMPERATURE**

MATERIAL	TEMPERATURE, °F								
	73	90	110	140	170	200	210	250	280
PVC	4.20	3.85	3.40	3.00	---	---	---	---	---
CPVC	4.23	4.10	3.70	3.27	2.93	2.40	2.26	---	---
PP Fuseal	2.00	1.30	.097	.074	0.61	0.55	0.53	---	---
PP Pressure	1.50	1.34	1.18	0.96	0.77	0.59	0.53	---	---
PVDF	2.13	1.66	1.37	1.04	0.80	0.61	0.55	0.37	0.29

**EXTERNAL PRESSURES - COLLAPSE RATING**

Thermoplastic pipe is frequently specified for situations where uniform external pressures are applied to the pipe, such as in underwater applications. In these applications, the collapse rating of the pipe determines the maximum permissible pressure differential between external and internal pressures. The basic formulas for collapsing external pressure applied uniformly to a long pipe are:

1. For thick wall pipe where collapse is caused by compression and failure of the pipe material:

$$P_c = \frac{o}{2D_o^2} (D_o^2 - D_i^2)$$

2. For thin wall pipe where collapse is caused by elastic instability of the pipe wall:

$$P_c = \frac{2cE}{1-\nu^2} \left( \frac{t}{D_m} \right)^3$$

**Where:**

- P<sub>c</sub> = Collapse Pressure (external minus internal pressure), psi
- o = Compressive Strength, psi
- E = Modulus of elasticity, psi
- ν = Poisson's Ratio
- D<sub>o</sub> = Outside Pipe Diameter, in.
- D<sub>m</sub> = Mean Pipe Diameter, in.
- D<sub>i</sub> = Inside Pipe Diameter, in.
- t = Wall Thickness, in.
- c = Out-of-Roundness Factor, Approximately 0.66

Choice of Formula - By using formula 2 on thick-wall pipe, an excessively large pressure will be obtained. It is therefore necessary to calculate, for a given pipe size, the collapse pressure using both formulas and use the lower value as a guide to safe working pressure. For short-term loading conditions, the values of E, o and ν from the relative properties charts shown on pages 40-41 will yield reasonable results. See individual materials charts for short-term collapse pressures at 73°F. For long-term loading conditions, appropriate long-term data should be used.

**SHORT-TERM COLLAPSE PRESSURE**

Thermoplastic pipe is often used for suction lines or in applications where external pressures are applied to the pipe, such as in heat exchangers, or underwater loading conditions. The differential pressure rating of the pipe between the internal and external pressures is determined by derating collapse pressures of the pipe. The differential pressure rating of the pipe is determined by derating the short-term collapse pressures shown in Table 19.

Collapse pressures must be adjusted for temperatures other than for room temperature. The pressure temperature correction chart (Table 19) used to adjust pipe pressure ratings may be used for this purpose. (See note below table).

**Table 19**

**SHORT-TERM COLLAPSE PRESSURE IN PSI AT 73°F**

1/2	3/4	1	1-1/4	1-1/2	2	3	4	6	8	10	12
<b>SCHEDULE 40 PVC</b>											
2095	1108	900	494	356	211	180	109	54	39	27	22
<b>SCHEDULE 80 PVC</b>											
2772	2403	2258	1388	927	632	521	335	215	147	126	117
<b>SCHEDULE 80 CPVC - IPS</b>											
2772	2403	2258	1388	927	632	521	335	215	147	126	117
<b>SCHEDULE 80 PRESSURE POLYPROPYLENE - IPS</b>											
1011	876	823	612	412	278	229	147	94	65	55	51
<b>SCHEDULE 80 PVDF - IPS</b>											
2936	1576	1205	680	464	309	255	164	105	72	61	57
<b>PROLINE PRO 150</b>											
40	40	40	40	40	40	40	40	40	40	40	40
<b>PROLINE PRO 45</b>											
1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6
<b>SUPER PROLINE</b>											
202	99	92	44	41	22	5.8	5.8	5.8	5.8	5.8	5.8

NOTE: These are short-term ratings; long-term ratings should be reduced by 1/3 to 1/2 of the short-term ratings.

**Vacuum Service - All sizes of Schedule 80 thermoplastic pipe are suitable for vacuum service up to 140°F and 30 inches of mercury.** Solvent-cemented joints are recommended for vacuum applications when using PVC. Schedule 40 PVC will handle full vacuum up to 24" diameter.

Laboratory tests have been conducted on Schedule 80 PVC pipe to determine performance under vacuum at temperatures above recommended operating conditions. Pipe sizes under 6 inches show no deformation at temperatures to 170°F and 27 inches of mercury vacuum.

The 6 inch pipe showed slight deformation at 165°F, and 20 inches of mercury. Above this temperature, failure occurred due to thread deformation.



# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## WATER HAMMER

Surge pressures due to water hammer are a major factor contributing to pipe failure in liquid transmission systems. A column of moving fluid within a pipeline, owing to its mass and velocity, contains stored energy. Since liquids are essentially incompressible, this energy cannot be absorbed by the fluid when a valve is suddenly closed. The result is a high momentary pressure surge, usually called water hammer. The five factors that determine the severity of water hammer are:

1. Velocity (The primary factor in excessive water hammer: see discussion of "Velocity" and "Safety Factor" on page 62).
2. Modulus of elasticity of material of which the pipe is made.
3. Inside diameter of pipe.
4. Wall thickness of pipe.
5. Valve closing time.

Maximum pressure surges caused by water hammer can be calculated by using the equation below. This surge pressure should be added to the existing line pressure to arrive at a maximum operating pressure figure.

$$P_s = V \left( \frac{E t 3960}{E t + 3 \times 10^5 D_i} \right)^{1/2}$$

Where:

- P<sub>s</sub> = Surge Pressure, in psi
- V = Liquid Velocity, in ft. per sec.
- D<sub>i</sub> = Inside Diameter of Pipe, in.
- E = Modulus of Elasticity of Pipe Material, psi
- t = Wall Thickness of Pipe, in.

Calculated surge pressure, which assumes instantaneous valve closure, can be calculated for any material using the values for E (Modulus of Elasticity) found in the properties chart, pages 13-14. Here are the most commonly used surge pressure tables for IPS pipe sizes.

**Table 20 - SURGE PRESSURE, P<sub>s</sub> IN PSI AT 73°F**

WATER VELOCITY (FT/SEC)	NOMINAL PIPE SIZE											
	1/2	3/4	1	1-1/4	1-1/2	2	3	4	6	8	10	12
<b>SCHEDULE 40 PVC &amp; CPVC</b>												
1	27.9	26.3	24.4	22.2	21.1	19.3	18.9	17.4	15.5	14.6	13.9	13.4
2	55.8	50.8	48.8	44.4	42.2	38.6	37.8	34.8	31.0	29.2	27.8	26.8
3	83.7	75.9	73.2	66.6	63.3	57.9	56.7	52.2	46.5	43.8	41.7	40.2
4	111.8	101.2	97.6	88.8	84.4	77.2	75.8	69.8	62.0	58.4	55.8	53.6
5	139.5	126.5	122.0	111.0	105.5	96.5	94.5	87.0	77.5	73.0	69.5	67.0
6	167.4	151.8	146.4	133.2	126.8	115.8	113.4	104.4	93.0	87.6	83.4	80.4
<b>SCHEDULE 80 PVC &amp; CPVC</b>												
1	32.9	29.9	28.7	26.2	25.0	23.2	22.4	20.9	19.4	18.3	17.3	17.6
2	65.6	59.8	57.4	52.4	50.0	46.4	44.8	41.8	38.8	36.6	35.6	35.2
3	98.7	89.7	86.7	78.8	75.0	69.6	67.2	62.7	56.2	52.9	50.4	48.8
4	131.6	119.6	114.8	104.8	101.0	92.8	89.8	83.6	73.6	69.2	65.2	62.4
5	164.5	149.5	143.5	131.0	125.0	118.0	112.0	104.5	91.0	85.5	80.0	76.0
6	197.4	179.4	172.2	157.2	150.0	133.2	134.4	125.4	116.4	109.8	106.8	106.6
<b>SCHEDULE 80 POYLPORYLENE</b>												
1	23.6	20.9	20.0	18.1	17.1	15.9	15.2	14.1	13.1	12.2	11.9	11.8
2	47.0	41.8	40.0	36.2	34.2	31.6	30.4	28.2	26.2	24.4	23.8	23.6
3	70.5	62.7	60.0	54.3	51.3	47.4	45.6	42.3	39.3	36.6	35.7	35.4
4	94.0	83.6	80.0	72.4	68.4	63.2	60.8	56.4	52.4	48.8	47.6	47.2
5	117.5	104.5	100.0	90.5	85.5	79.0	76.0	70.5	65.5	61.0	59.5	59.0
6	141.0	125.4	120.0	108.6	102.6	94.8	91.2	84.6	78.6	73.2	71.4	70.8
<b>SCHEDULE 80 PVDF</b>												
1	26.2	22.6	21.6	19.5	18.5	17.1	16.5	15.3	14.2	13.3	12.9	12.8
2	50.4	45.2	43.2	39.0	37.0	34.2	33.0	30.6	28.9	26.8	25.8	25.6
3	75.6	67.8	64.8	58.5	55.5	51.3	49.5	45.9	42.6	39.9	38.7	38.4
4	100.8	90.4	86.4	78.0	74.0	68.4	66.0	61.2	56.8	53.2	51.6	51.2
5	126.0	118.0	108.0	97.5	92.5	86.5	82.5	76.5	71.0	66.5	64.5	64.0
6	151.2	135.6	129.6	117.0	111.0	102.8	99.0	91.8	85.2	79.8	77.4	76.8
<b>SUPER PROLINE</b>												
1	22.3	19.8	19.6	17.4	17.1	15.5	14.4	12.6	12.5	12.4	12.4	12.4
2	44.5	39.7	39.1	34.7	34.2	30.9	24.8	26.2	24.9	24.8	24.9	24.8
3	66.8	59.5	58.7	52.1	51.4	46.4	37.2	37.7	37.4	37.2	37.3	37.3
4	89.1	79.4	78.3	69.5	68.5	61.8	49.7	50.3	49.9	49.6	49.8	49.7
5	111.3	99.2	97.9	86.9	85.6	77.3	62.1	62.9	62.3	62.0	62.2	62.1
6	133.6	119.0	117.4	104.2	102.7	92.8	74.5	75.5	74.8	74.4	74.6	74.5
<b>PROLINE PRO 150</b>												
1	15.3	14.1	12.9	12.6	12.8	12.8	12.7	12.7	12.8	12.7	12.7	12.7
2	30.7	28.2	25.9	25.3	26.6	25.6	25.5	25.4	25.5	25.5	25.5	25.5
3	46.0	42.3	38.8	37.9	38.4	38.4	38.2	38.2	38.3	38.2	38.2	38.2
4	61.4	56.4	51.8	50.5	51.2	51.2	51.0	50.9	51.0	50.9	51.0	50.9
5	76.7	70.5	64.7	63.2	64.0	64.0	63.7	63.6	63.8	63.7	63.7	63.7
6	92.1	84.8	77.6	75.8	76.8	76.8	76.5	76.3	76.5	76.4	76.5	76.4
<b>PROLINE PRO 45</b>												
1	-	-	-	-	-	7.1	7.0	7.1	7.1	7.0	7.1	7.1
2	-	-	-	-	-	14.2	14.1	14.3	14.2	14.1	14.1	14.1
3	-	-	-	-	-	21.3	21.1	21.4	21.2	21.1	21.2	21.1
4	-	-	-	-	-	28.4	28.1	28.6	28.3	28.2	28.2	28.2
5	-	-	-	-	-	35.5	35.2	35.7	35.4	35.2	35.3	35.3
6	-	-	-	-	-	42.5	42.3	42.8	42.5	42.2	42.4	42.3

NOTE: For sizes larger than 12", call your Corr Tech representative.



# SYSTEMS ENGINEERING DATA

## FOR THERMOPLASTIC PIPING

### WATER HAMMER (continued)

However, to keep water hammer pressures within reasonable limits, it is common practice to design valves for closure times considerably greater than  $2L/C$ .

$$T_c > \frac{2L}{C}$$

**Where:**  $T_c$  = Valve Closure time, sec.  
 $L$  = Length of Pipe run, ft.  
 $C$  = Sonic Velocity of the Pressure Wave = 4720 ft. sec.

Another formula which closely predicts water hammer effects is:

$$p = a \frac{w}{144g}$$

Which is based on the elastic wave theory. In this text, we have further simplified the equation to:

$$p = Cv$$

**Where:**  $p$  = maximum surge pressure, psi  
 $v$  = fluid velocity in feet per second  
 $C$  = surge wave constant for water at 73°F

It should be noted that the surge pressure (water hammer) calculated here is a maximum pressure rise for any fluid velocity, such as would be expected from the instant closing of a valve. It would therefore yield a somewhat conservative figure for use with slow closing actuated valves, etc.

For fluids heavier than water, the following correction should be made to the surge wave constant  $C$ .

$$C^1 = \frac{(S.G. - 1) C + C}{2}$$

**Where:**  $C^1$  = Corrected Surge Wave Constant  
 S.G. = Specific Gravity or Liquid

For example, for a liquid with a specific gravity of 1.2 in 2" Schedule 80 PVC pipe, from Table 43 = 24.2

$$C^1 = \frac{(1.2 - 1)(24.2) + 24.2}{2}$$

$$C^1 = 2.42 + 24.2$$

$$C^1 = 26.6$$

**Table 21 - Surge Wave Correction for Specific Gravity**

PIPE SIZE (IN.)	PVC		CPVC		POLY-PROPYLENE (PVDF) SCH 80	KYNAR (PVDF) SCH 80
	SCH 40	SCH 80	SCH 40	SCH 80		
1/4	31.3	34.7	33.2	37.3	—	—
3/8	29.3	32.7	31.0	34.7	—	—
1/2	28.7	31.7	30.3	33.7	25.9	28.3
3/4	26.3	29.8	27.8	31.6	23.1	25.2
1	25.7	29.2	27.0	30.7	21.7	24.0
1-1/4	23.2	27.0	24.5	28.6	19.8	—
1-1/2	22.0	25.8	23.2	27.3	18.8	20.6
2	20.2	24.2	21.3	25.3	17.3	19.0
2-1/2	21.1	24.7	22.2	26.0	—	—
3	19.5	23.2	20.6	24.5	16.6	—
4	17.8	21.8	18.8	22.9	15.4	—
6	15.7	20.2	16.8	21.3	—	—
8	14.8	18.8	15.8	19.8	—	—
10	14.0	18.3	15.1	19.3	—	—
12	13.7	18.0	14.7	19.2	—	—
14	13.4	17.9	14.4	19.2	—	—

### Proper design when laying out a piping system will eliminate the possibility of water hammer damage.

The following suggestions will help in avoiding problems:

- 1) In a plastic piping system, a fluid velocity not exceeding 5ft/sec. will minimize water hammer effects, even with quickly closing valves, such as solenoid valves.
- 2) Using actuated valves which have a specific closing time will eliminate the possibility of someone inadvertently slamming a valve open or closed too quickly. With pneumatic and air-spring actuators, it may be necessary to place a valve in the air line to slow down the valve operation cycle.
- 3) If possible, when starting a pump, partially close the valve in the discharge line to minimize the volume of liquid which is rapidly accelerating through the system. Once the pump is up to speed and the line completely full, the valve may be opened.
- 4) A check valve installed near a pump in the discharge line will keep the line full and help prevent excessive water hammer during pump start-up.

### VELOCITY

Thermoplastic piping systems have been installed that have successfully handled water velocities in excess of 10 ft/sec. Thermoplastic pipe is not subject to erosion caused by high velocities and turbulent flow, and in this respect is superior to metal piping systems, particularly where corrosive or chemically aggressive fluids are involved. The Plastics Pipe Institute has issued the following policy statement on water velocity: The maximum safe water velocity in a thermoplastic piping system depends on the specific details of the system and the operating conditions. **In general, 5 feet per second is considered to be safe.** Higher velocities may be used in cases where the operating characteristics of valves and pumps are known so that sudden changes in flow velocity can be controlled. The total pressure in the system at any time (operating plus surge or water hammer) should not exceed 150 percent of the pressure rating of the system.

### SAFETY FACTOR

As the duration of pressure surges due to water hammer is extremely short - seconds, or more likely, fractions of a second - in determining the safety factor the maximum fiber stress due to total internal pressure must be compared to some very short-term strength value. Referring to Figure 2, shown on page 15, it will be seen that the failure stress for very short time periods is very high when compared to the hydrostatic design stress. The calculation of safety factor may thus be based very conservatively on the 20-second strength value given in Figure 2, shown on page 15 - 8470 psi for PVC Type 1.

A sample calculation is shown below, based upon the listed criteria:

Pipe = 1-1/4" Schedule 80 PVC  
 O.D. = 1.660: Wall = 0.191  
 HDS = 2000 psi

The calculated surge pressure for 1-1/4" Schedule 80 PVC pipe at a velocity of 1 ft/sec is 26.2 psi/ft/sec.

# CARRYING CAPACITY & FRICTION LOSS

## TABLE 22

### CARRYING CAPACITY AND FRICTION LOSS FOR SCHEDULE 80 THERMOPLASTIC PIPE

(Independent variables: Gallons per minute and nominal pipe size O.D.)

Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth.)

GALLONS PER MINUTE	1/2 IN.			3/4 IN.			1 IN.			1-1/4 IN.			1-1/2 IN.			2 IN.			2-1/2 IN.			3 IN.		
	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH
1	1.48	4.02	1.74	0.74	0.86	0.37	0.94	0.88	0.38	0.52	0.21	0.09	0.38	0.10	0.041	0.56	0.10	0.040	0.39	0.05	0.022	0.25	0.02	0.009
2	2.96	8.03	3.48	1.57	1.72	0.74	2.34	2.75	1.19	1.30	0.66	0.29	0.94	0.30	0.126	1.12	0.20	0.080	0.78	0.10	0.032	0.50	0.04	0.017
5	7.39	45.23	19.59	3.92	9.67	4.19	3.28	5.04	2.19	1.82	1.21	0.53	1.32	0.55	0.24	1.12	0.29	0.13	0.78	0.12	0.052	1.00	0.04	0.017
7	10.34	83.07	35.97	5.49	17.76	7.69	4.68	9.61	4.16	2.60	2.30	1.00	1.98	1.04	0.45	1.12	0.29	0.13	0.78	0.12	0.052	1.00	0.04	0.017
10				7.84	33.84	14.65				3.90	4.87	2.11	2.81	2.20	0.95	1.68	0.62	0.27	1.17	0.26	0.11	0.75	0.09	0.039
15				11.76	71.70	31.05				7.01	20.36	8.82	4.69	5.67	2.46	2.23	1.06	0.46	1.56	0.44	0.19	1.00	0.15	0.065
20				0.57	0.04	0.017	9.35	34.68	15.02	5.20	8.30	3.59	5.63	7.95	3.44	3.35	2.25	0.97	2.34	0.94	0.41	1.49	0.31	0.13
25				0.72	0.06	0.026	11.69	52.43	22.70	6.50	12.55	5.43	6.57	10.58	4.58	3.91	2.99	1.29	2.73	1.25	0.54	1.74	0.42	0.18
30				0.86	0.08	0.035	0.54	0.03	0.013	14.03	73.48	31.82	8.57	10.58	4.58	4.47	3.83	1.86	3.12	1.60	0.69	1.99	0.54	0.23
35				1.00	0.11	0.048	0.63	0.04	0.017				10.40	29.97	12.98	7.50	13.55	5.87	4.47	3.83	1.86	3.12	1.60	0.69
40				1.15	0.14	0.061	0.72	0.04	0.017	10.40	29.97	12.98	11.70	37.27	16.14	8.44	16.85	7.30	5.03	4.76	2.07	3.51	1.99	0.86
45				1.29	0.17	0.074	0.81	0.06	0.026	11.70	37.27	16.14	13.00	45.30	19.61	9.38	20.48	8.87	5.58	5.79	2.51	3.90	2.42	1.05
50				1.43	0.21	0.091	0.90	0.07	0.030	13.00	45.30	19.61	11.26	28.70	12.43	11.26	28.70	12.43	6.70	8.12	3.52	4.68	3.39	1.47
60				1.72	0.30	0.13	1.08	0.10	0.043	0.75	0.04	0.017							7.82	10.80	4.68	5.46	4.51	1.95
70				2.01	0.39	0.17	1.26	0.13	0.056	0.88	0.05	0.022							8.38	12.27	5.31	5.85	5.12	2.22
75				2.15	0.45	0.19	1.35	0.14	0.061	0.94	0.06	0.026							8.93	13.83	5.99	6.24	5.77	2.50
80				2.29	0.50	0.22	1.44	0.16	0.069	1.00	0.07	0.030							9.48	15.48	6.66	6.72	6.43	2.81
90				2.58	0.63	0.27	1.62	0.20	0.087	1.13	0.08	0.035							10.06	17.20	7.45	7.02	7.18	3.11
100				2.87	0.76	0.33	1.80	0.24	0.10	1.25	0.10	0.043							10.66	19.06	8.34	7.60	8.02	3.48
125				3.59	1.16	0.50	2.25	0.37	0.16	1.57	0.16	0.068							11.17	20.90	9.05	8.17	9.02	3.84
150				4.30	1.61	0.70	2.70	0.52	0.23	1.86	0.22	0.095							11.70	22.81	9.95	8.75	10.00	4.23
175				5.02	2.15	0.93	3.15	0.69	0.30	2.20	0.29	0.12							12.27	24.81	10.95	9.38	10.57	4.58
200				5.73	2.75	1.19	3.60	0.88	0.38	2.51	0.37	0.16							12.84	26.90	12.05	10.00	11.14	4.93
250				7.16	4.16	1.81	4.50	1.34	0.58	3.14	0.56	0.24							13.42	29.08	13.25	10.66	11.74	5.38
300				8.60	5.83	2.52	5.40	1.87	0.81	3.76	0.78	0.34							14.00	31.35	14.55	11.27	12.43	5.83
350				10.03	7.76	3.36	6.30	2.49	1.08	4.39	1.04	0.45							14.58	33.71	15.90	11.89	13.12	6.38
400				11.47	9.93	4.30	7.19	3.19	1.38	5.02	1.33	0.58							15.17	36.16	17.25	12.56	13.90	6.93
450							8.09	3.97	1.72	5.64	1.65	0.71							15.76	38.70	18.65	13.27	14.71	7.50
500							8.99	4.82	2.09	6.27	2.00	0.87							16.36	41.31	19.70	14.00	15.52	8.09
750							9.40	4.25	1.84	9.40	4.25	1.84							17.56	46.88	22.22	15.11	16.43	8.93
1000							12.54	7.23	3.13	12.54	7.23	3.13							18.72	53.46	25.75	15.74	17.38	9.88
1250							8.93	2.78	1.20	8.93	2.78	1.20							19.31	56.13	28.28	16.00	18.33	10.83
1500							10.71	3.89	1.68	10.71	3.89	1.68							19.90	58.89	30.80	16.27	19.38	11.78
2000																			20.48	61.74	33.41	16.52	20.43	12.73
2500																			21.07	64.67	36.02	16.77	21.48	13.68
3000																			21.66	67.68	38.63	17.02	22.53	14.63
3500																			22.25	70.77	41.24	17.27	23.58	15.58
4000																			22.84	73.93	43.85	17.52	24.63	16.53

# CARRYING CAPACITY & FRICTION LOSS

## TABLE 23

### CARRYING CAPACITY AND FRICTION LOSS FOR SCHEDULE 40 THERMOPLASTIC PIPE

(Independent variables: Gallons per minute and nominal pipe size O. D.  
 Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth.)

GALLONS PER MINUTE	1/2 IN.			3/4 IN.			1 IN.			1-1/4 IN.			1-1/2 IN.			2 IN.			2-1/2 IN.			3 IN.		
	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICTION HEAD FEET	FRICTION LOSS POUNDS PER SQUARE INCH
1	7.13	2.06	0.90	0.63	0.51	0.22	0.77	0.55	0.24	0.44	0.14	0.06	0.33	0.07	0.03	0.49	0.066	0.020	0.30	0.038	0.016	0.22	0.015	0.007
2	2.26	4.16	1.80	1.26	1.02	0.44	1.93	1.72	0.75	1.11	0.44	0.19	0.81	0.22	0.09	0.89	0.11	0.048	0.49	0.051	0.023	0.31	0.021	0.009
5	5.64	23.44	10.15	3.16	5.73	2.48	2.72	3.17	1.37	1.55	0.81	0.35	1.13	0.38	0.17	0.89	0.21	0.091	0.68	0.09	0.039	0.44	0.03	0.013
7	7.90	43.06	13.64	4.43	10.52	4.56	3.86	6.02	2.61	2.21	1.55	0.67	1.62	0.72	0.31	0.98	0.21	0.091	1.03	0.19	0.082	0.66	0.07	0.030
10	11.28	82.02	35.51	6.32	20.04	8.68	5.79	12.77	5.53	3.31	3.28	1.42	2.42	1.53	0.66	1.46	0.45	0.19	1.03	0.19	0.082	0.66	0.07	0.030
15	20	0.51	0.013	12.85	72.34	31.32	7.72	21.75	9.42	4.42	5.59	2.42	3.23	2.61	1.13	1.95	0.76	0.33	1.37	0.32	0.14	0.88	0.11	0.048
25	0.64	0.04	0.017	5.52	8.45	3.66	9.65	32.89	14.22	5.52	8.45	3.66	4.04	3.95	1.71	2.44	1.15	0.50	1.71	0.49	0.21	1.10	0.17	0.074
30	0.77	0.06	0.026	6.63	11.85	5.13	11.58	46.08	19.95	6.63	11.85	5.13	4.85	5.53	2.39	2.93	1.62	0.70	2.05	0.68	0.29	1.33	0.23	0.10
35	0.89	0.08	0.035	7.73	15.76	6.82	7.73	15.76	6.82	7.73	15.76	6.82	5.66	7.36	3.19	3.41	2.15	0.93	2.39	0.91	0.39	1.55	0.31	0.13
40	1.02	0.11	0.048	8.84	20.18	8.74	8.84	20.18	8.74	8.84	20.18	8.74	6.47	9.43	4.08	3.90	2.75	1.19	2.73	1.16	0.50	1.77	0.40	0.17
45	1.15	0.13	0.056	9.94	25.10	10.87	9.94	25.10	10.87	9.94	25.10	10.87	7.27	11.73	5.08	4.39	3.43	1.49	3.00	1.44	0.62	1.99	0.50	0.22
50	1.28	0.16	0.069	11.05	30.51	13.21	11.05	30.51	13.21	11.05	30.51	13.21	8.08	14.25	6.17	4.88	4.16	1.80	3.42	1.75	0.76	2.21	0.60	0.26
60	1.53	0.22	0.095	0.67	0.03	0.013	0.67	0.03	0.013	0.67	0.03	0.013	9.70	19.98	8.65	5.85	5.84	2.53	4.10	2.46	1.07	2.65	0.85	0.37
70	1.79	0.30	0.13	0.79	0.04	0.017	0.79	0.04	0.017	0.79	0.04	0.017	8.65	19.98	8.65	6.53	7.76	3.36	4.79	3.27	1.42	3.09	1.13	0.49
75	1.92	0.34	0.15	0.84	0.05	0.022	0.84	0.05	0.022	0.84	0.05	0.022	9.70	19.98	8.65	7.32	8.82	3.82	5.13	3.71	1.61	3.31	1.28	0.55
80	2.05	0.38	0.16	0.90	0.05	0.022	0.90	0.05	0.022	0.90	0.05	0.022	10.87	19.98	8.65	7.90	9.94	4.30	5.47	4.19	1.81	3.53	1.44	0.62
90	2.30	0.47	0.20	1.01	0.06	0.026	1.01	0.06	0.026	1.01	0.06	0.026	11.73	19.98	8.65	8.78	12.37	5.36	6.35	5.21	2.26	3.98	1.80	0.76
100	2.56	0.58	0.25	1.12	0.08	0.035	1.12	0.08	0.035	1.12	0.08	0.035	12.73	19.98	8.65	9.75	15.03	6.51	6.84	6.33	2.74	4.42	2.18	0.94
125	3.20	0.88	0.38	1.41	0.12	0.052	1.41	0.12	0.052	1.41	0.12	0.052	14.25	19.98	8.65	9.75	15.03	6.51	8.58	9.58	4.35	5.52	3.31	1.43
150	3.84	1.22	0.53	1.69	0.16	0.069	1.69	0.16	0.069	1.69	0.16	0.069	15.76	19.98	8.65	10.87	19.98	8.65	10.87	13.41	5.81	6.63	4.93	2.00
175	4.48	1.63	0.71	1.97	0.22	0.096	1.97	0.22	0.096	1.97	0.22	0.096	17.33	19.98	8.65	12.37	19.98	8.65	12.37	16.16	6.16	7.73	6.16	2.67
200	5.11	2.08	0.90	2.25	0.28	0.12	2.25	0.28	0.12	2.25	0.28	0.12	19.98	19.98	8.65	14.25	19.98	8.65	14.25	19.98	6.16	8.83	7.88	3.47
250	6.40	3.15	1.36	2.81	0.43	0.19	2.81	0.43	0.19	2.81	0.43	0.19	23.95	19.98	8.65	18.18	19.98	8.65	18.18	19.98	6.16	11.04	11.93	5.17
300	7.67	4.41	1.91	3.37	0.60	0.26	3.37	0.60	0.26	3.37	0.60	0.26	27.33	19.98	8.65	21.17	19.98	8.65	21.17	19.98	6.16	13.41	14.43	6.16
350	8.95	5.87	2.55	3.94	0.79	0.34	3.94	0.79	0.34	3.94	0.79	0.34	30.51	19.98	8.65	24.17	19.98	8.65	24.17	19.98	6.16	16.16	17.33	6.16
400	10.23	7.52	3.26	4.49	1.01	0.44	4.49	1.01	0.44	4.49	1.01	0.44	34.31	19.98	8.65	27.17	19.98	8.65	27.17	19.98	6.16	19.98	21.17	6.16
450				5.06	1.26	0.55	5.06	1.26	0.55	5.06	1.26	0.55	38.26	19.98	8.65	31.17	19.98	8.65	31.17	19.98	6.16	23.95	26.16	6.16
500				6.12	3.76	1.63	6.12	3.76	1.63	6.12	3.76	1.63	43.06	19.98	8.65	35.17	19.98	8.65	35.17	19.98	6.16	28.17	31.17	6.16
750				8.43	3.25	1.41	8.43	3.25	1.41	8.43	3.25	1.41	60.87	19.98	8.65	48.17	19.98	8.65	48.17	19.98	6.16	35.17	38.26	6.16
1000				11.24	5.54	2.40	11.24	5.54	2.40	11.24	5.54	2.40	81.17	19.98	8.65	63.17	19.98	8.65	63.17	19.98	6.16	43.06	46.16	6.16
1250				8.11	2.20	0.95	8.11	2.20	0.95	8.11	2.20	0.95	100.87	19.98	8.65	76.17	19.98	8.65	76.17	19.98	6.16	51.17	54.26	6.16
1500				9.72	3.07	1.33	9.72	3.07	1.33	9.72	3.07	1.33	120.87	19.98	8.65	91.17	19.98	8.65	91.17	19.98	6.16	59.17	62.26	6.16
2000				8.21	1.72	0.74	8.21	1.72	0.74	8.21	1.72	0.74	150.87	19.98	8.65	106.17	19.98	8.65	106.17	19.98	6.16	67.17	70.26	6.16
2500				10.27	2.61	1.13	10.27	2.61	1.13	10.27	2.61	1.13	180.87	19.98	8.65	121.17	19.98	8.65	121.17	19.98	6.16	75.17	78.26	6.16
3000				8.68	1.55	0.67	8.68	1.55	0.67	8.68	1.55	0.67	210.87	19.98	8.65	136.17	19.98	8.65	136.17	19.98	6.16	83.17	86.26	6.16
3500				10.12	2.07	0.90	10.12	2.07	0.90	10.12	2.07	0.90	240.87	19.98	8.65	151.17	19.98	8.65	151.17	19.98	6.16	91.17	94.26	6.16
4000				11.07	2.86	1.15	11.07	2.86	1.15	11.07	2.86	1.15	270.87	19.98	8.65	166.17	19.98	8.65	166.17	19.98	6.16	99.17	102.26	6.16

# PROLINE-POLYPROPYLENE 150 FLOW RATES

TABLE 24

GALLONS PER MINUTE	1/2 IN.			3/4 IN.			1 IN.			1-1/4 IN.			1-1/2 IN.			2 IN.			2-1/2 IN.			3 IN.			4 IN.			
	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICITION HEAD FEET	FRICITION LOSS POUNDS PER SQUARE INCH	
1	1.17	1.27	.55	.66	.35	.15	.39	.09	.04	.24	.02	.01	.32	.05	.02	.50	.07	.03	.38	.02	.01	.24	.02	.01	.24	.02	.01	
2	2.34	4.60	1.99	1.37	1.25	.54	.76	.32	.14	.49	.09	.04	1.22	.55	.24	.79	.18	.06	.79	.05	.02	.48	.05	.02	.48	.05	.02	
5	5.84	25.04	10.84	3.42	6.81	2.95	1.95	1.73	.75	1.22	1.04	.45	1.11	.37	.16	1.70	.12	.05	.49	.05	.02	.34	.05	.02	.34	.05	.02	
7	8.16	46.88	20.21	4.79	12.73	5.51	2.72	3.21	1.39	1.71	1.04	.45	1.58	.69	.30	2.45	.23	.10	.70	.09	.04	.49	.07	.03	.49	.07	.03	
10	11.70	90.37	39.12	6.85	24.62	10.66	3.89	6.24	2.70	2.45	2.01	.87	1.58	.69	.30	3.48	.23	.10	.70	.09	.04	.49	.07	.03	.49	.07	.03	
15				10.30	52.18	22.59	5.84	13.21	5.72	3.67	4.27	1.85	2.37	1.48	.64	5.53	.70	.30	1.00	.24	.09	.43	.14	.06	.49	.02	.01	
20				7.78	22.50	8.74	4.90	7.28	3.15	3.16	2.52	1.09	1.99	.83	.36	1.41	.35	.15	1.41	.35	.15	.97	.23	.10	.65	.05	.02	
25				8.73	34.00	14.72	6.12	11.02	4.77	6.12	11.02	4.77	3.95	3.79	1.64	2.48	1.25	.54	1.76	.53	.23	1.22	.30	.13	.81	.07	.03	
30				11.70	47.06	20.03	8.57	20.54	8.89	8.57	20.54	8.89	5.53	7.09	3.07	3.48	2.31	1.00	2.48	.99	.43	1.70	.53	.23	1.14	.14	.06	
35	.54	.02	.01																									
40	.62	.05	.02																									
45	.69	.05	.02																									
50	.77	.07	.03																									
60	.92	.07	.03																									
70	1.08	.09	.04																									
80	1.23	.12	.05																									
90	1.39	.14	.06																									
100	1.54	.16	.07																									
125	1.92	.25	.11																									
150	2.31	.37	.16																									
175	2.69	.49	.21																									
200	3.08	.62	.27																									
250	3.85	.92	.40																									
300	4.62	1.32	.57																									
350	5.39	1.73	.75																									
400	6.15	2.24	.97																									
450	6.93	2.77	1.20																									
500	7.69	3.37	1.46																									
600	9.23	4.71	2.04																									
700	10.80	6.28	2.72																									
800				6.89	2.13	.92	4.41	.72	.31	2.78	.23	.10	2.19	.14	.06	1.72	.07	.03	1.36	.05	.02							
900				7.87	2.70	1.17	5.04	.92	.40	3.17	.30	.13	2.50	.16	.07	1.97	.09	.04	1.55	.05	.02							
1000				8.85	3.37	1.46	5.67	1.13	.49	3.57	.37	.15	2.81	.21	.09	2.21	.12	.05	1.75	.07	.03							
2000				9.84	4.11	1.78	6.30	1.39	.60	3.97	.44	.19	3.12	.25	.11	2.45	.14	.06	1.94	.07	.03							
2500				12.60	5.01	2.17	12.60	5.01	2.17	7.93	1.62	.70	6.24	.90	.39	4.92	.51	.22	3.88	.30	.13							
5000																												
7500																												

# PROLINE-POLYPROPYLENE 45 FLOW RATES

**TABLE 25**

GALLONS PER MINUTE	2 IN.			2-1/2 IN.			3 IN.			4 IN.			6 IN.			8 IN.			10 IN.			12 IN.			14 IN.				
	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH	VELOCITY FEET PER SECOND	FRICION HEAD FEET	FRICION LOSS POUNDS PER SQUARE INCH		
5	.38	.09	.01	.37	.08	.01	.37	.02	.01	.50	.02	.01																	
7	.53	.07	.00	.53	.06	.02	.53	.05	.02																				
10	.76	.12	.00	.76	.10	.03	.76	.05	.02																				
15	1.13	.23	.10	1.07	.18	.06	1.07	.07	.03																				
20	1.51	.42	.16	1.07	.18	.06	1.07	.07	.03																				
25	1.89	.62	.27	1.34	.28	.12	1.34	.12	.05	.60	.05	.02																	
30	2.27	.86	.36	1.60	.37	.16	1.11	.14	.06	.74	.07	.03																	
35	2.64	1.16	.51	1.87	.51	.22	1.29	.21	.09	.87	.07	.03																	
40	3.02	1.50	.66	2.14	.65	.28	1.48	.25	.11	.98	.09	.04																	
45	3.40	1.87	.81	2.40	.81	.35	1.66	.32	.14	1.12	.12	.05																	
50	3.78	2.29	.99	2.67	.97	.43	1.84	.40	.17	1.24	.14	.06	.70	.02	.01														
60	4.53	3.19	1.38	3.30	1.35	.58	2.32	.55	.24	1.69	.21	.09	.82	.05	.02														
70	5.29	4.25	1.84	3.74	1.82	.75	2.69	.74	.32	1.74	.28	.12	.82	.05	.02														
80	6.04	5.43	2.35	4.27	2.38	1.03	3.06	.95	.41	1.89	.37	.16	.84	.07	.03														
90	6.80	6.77	2.93	4.80	2.91	1.26	3.33	1.20	.52	2.23	.44	.19	1.03	.07	.03														
100	7.55	8.22	3.56	5.34	3.53	1.53	3.69	1.43	.62	2.48	.50	.24	1.17	.09	.04														
125	9.44	12.43	5.38	6.68	5.41	2.34	4.82	2.17	.96	3.10	.63	.36	1.45	.14	.06	.90	.02	.01											
150	11.30			8.01	7.46	3.24	5.54	3.07	1.30	3.72	1.16	.50	1.76	.18	.08	1.12	.07	.03											
175				9.35	9.96	4.31	6.47	4.07	1.70	4.34	1.50	.67	2.05	.25	.11	1.31	.07	.03	.84	.02	.01								
200				10.68	12.77	5.53	7.59	5.22	2.26	4.96	1.89	.86	2.34	.32	.14	1.50	.07	.03	.96	.05	.02								
250							9.94	7.88	3.41	6.20	2.88	1.29	2.92	.49	.21	1.87	.12	.05	1.20	.05	.02								
300							11.08	11.04	4.78	7.44	4.18	1.81	3.51	.67	.29	2.24	.15	.07	1.44	.07	.03								
350										8.58	5.03	2.42	4.10	.90	.39	2.62	.23	.10	1.68	.09	.04	1.06	.02	.01					
400										9.93	7.14	3.09	4.66	1.18	.50	2.99	.30	.13	1.92	.14	.06	1.21	.05	.02					
450										11.17	8.87	3.84	5.27	1.43	.62	3.37	.37	.16	2.16	.16	.07	1.38	.05	.02	1.07	.02			
500	1.12	.02	.01							5.65	1.73	.75	5.65	1.73	.75	3.74	.44	.19	2.40	.21	.09	1.51	.07	.03	1.19	.05			
600	1.31	.05	.02							7.02	2.43	1.05	4.49	.60	.26	2.87	.28	.12	1.81	.28	.12	1.81	.28	.12	1.81	.28	.12	1.81	.28
700	1.50	.09	.02							8.19	3.23	1.40	5.24	.83	.36	3.35	.35	.15	2.11	.35	.15	2.11	.35	.15	2.11	.35	.15	2.11	.35
800	1.68	.07	.02							9.36	4.13	1.79	5.96	1.04	.45	3.83	.45	.20	2.41	.45	.20	2.41	.45	.20	2.41	.45	.20	2.41	.45
900	1.87	.07	.03							10.53	5.15	2.23	6.73	1.29	.60	4.31	.60	.30	2.71	.60	.30	2.71	.60	.30	2.71	.60	.30	2.71	.60
1000	1.67	.07	.03							11.70	6.26	2.71	7.48	1.57	.68	4.79	.72	.31	3.02	.72	.31	3.02	.72	.31	3.02	.72	.31	3.02	.72
2000	3.74	.25	.11	2.96	.14	.06	2.39	.09	.04	1.51	.02	.01																	
2500	4.67	.39	.17	3.69	.23	.10	2.98	.14	.06	1.89	.05	.02																	
5000	9.35	1.41	.61	7.38	.91	.35	5.96	.48	.21	3.77	.16	.07																	
7500	14.00	.88	.30	11.00	1.71	.74	8.97	1.02	.44	5.66	.32	.14																	
10000				14.80	2.91	1.26	12.00	1.73	.70	7.55	.55	.24																	



# CARRYING CAPACITY & FRICTION LOSS

## TABLE 27

### EQUIVALENT LENGTH OF THERMOPLASTIC PIPE IN FEET

	1/4"	3/8"	1/2"	5/8"	1"	1 1/4"	1 1/2"	2"	2 1/2"	3"	4"	6"	8"	10"	12"			
<b>GLOBE VALVES</b>	With no obstruction in flat, bevel, or plug type seat		Fully Open		10.3	17.6	23.3	29.7	39.1	45.6	58.6	69.95	86.9	114.1	171.8	226.1	283.9	338.2
	With wing or pin guided disc		Fully Open		13.7	23.3	30.9	39.3	51.8	60.4	77.5	92.5	115.1	151.0	227.4	299.3	375.8	447.7
<b>ANGLE VALVES</b>	(No obstruction in flat, bevel or plug type seat)		Fully Open		5.3	9.1	12.0	15.3	20.1	23.5	30.1	36.0	44.7	58.7	80.4	116.4	146.1	174.1
	With stem 60 degrees from run of pipe line		Fully Open		4.4	7.5	10.0	12.7	16.7	19.5	25.0	29.8	37.1	48.6	73.3	96.4	121.1	144.3
<b>GATE VALVES</b>	With no obstruction in flat, bevel, plug type seat		Fully Open		4.4	7.5	10.0	12.7	16.7	19.5	25.0	29.8	37.1	48.6	73.3	96.4	121.1	144.3
	With wing or pin guided disc		Fully Open		6.1	10.4	13.7	17.5	23.0	26.8	34.5	41.2	51.1	67.1	101.1	133.0	167.0	199.0
<b>BALL VALVES</b>	Conventional		Fully Open		0.4	0.7	0.9	1.1	1.5	1.7	2.2	2.7	3.3	4.4	6.6	8.6	10.9	12.9
	Wedge Disc, Dbl Disc, or Plug Disc		Three-Quarters Open		1.1	1.8	2.4	3.1	4.0	4.7	6.0	7.2	8.9	11.7	17.7	23.3	29.2	34.8
			One-Half Open		4.9	8.3	11.0	14.0	18.4	21.5	27.6	32.9	40.9	53.7	80.9	106.4	133.6	159.2
			One-Quarter Open		27.3	45.7	61.8	78.7	103.5	120.8	155.0	185.2	230.1	302.0	454.9	598.6	751.5	895.4
<b>FITTINGS</b>	Full Port Design		Fully Open		Same as an equivalent of Sch. 80 Pipe													
	90° Standard Elbow				0.9	1.6	2.1	2.6	3.5	4.0	5.5	6.2	7.7	10.1	15.2	20.0	25.1	29.8
	45° Standard Elbow				0.5	0.8	1.1	1.4	1.8	2.1	2.8	3.3	4.1	5.4	8.1	10.6	13.4	15.9
<b>FITTINGS</b>	90° Long Radius Elbow				0.6	1.0	1.4	1.7	2.3	2.7	4.3	5.1	6.3	8.3	12.5	16.5	20.7	24.7
	90° Street Elbow				1.5	2.6	3.4	4.4	5.8	6.7	8.6	10.3	12.8	16.8	25.3	33.3	41.8	49.78
	45° Street Elbow				0.8	1.3	1.8	2.3	3.0	3.5	4.5	5.4	6.6	8.7	13.1	17.3	21.7	25.9
<b>FITTINGS</b>	Square Corner Elbow				1.7	3.0	3.9	5.0	6.5	7.6	9.8	11.7	14.6	19.1	26.8	37.9	47.6	56.7
	Standard Tee		With Flow through run		0.6	1.0	1.4	1.7	2.3	2.7	4.3	5.1	6.3	8.3	12.5	16.5	20.7	24.7
<b>FITTINGS</b>			With Flow through branch		1.8	4.0	5.1	6.0	6.9	8.1	12	14.3	16.3	22.1	32.2	39.9	50.1	59.7

# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

Water Velocity = 5 feet per second  
 Static Pressure in System = 300 psi  
 Total System Pressure = Static Pressure + Surge Pressure:  
 $P_t = P \times P_s$   
 $= 300 + 5 \times 26.2$   
 $= 431.0$  psi

Maximum circumferential stress is calculated from a variation of the ISO Equation:

$$S = \frac{P_t (D_o - t)}{2t} = \frac{431(1.660 - .191)}{2 \times .191} = 1657.4$$

$$\text{Safety Factor} = \frac{20 \text{ second strength}}{\text{Maximum stress}} = \frac{8470}{1657} = 5.11$$

Table 28 gives the results of safety factor calculations based upon service factors of 0.5 and 0.4 for the 1-1/4" PVC Schedule 80 pipe of the example shown above using the full pressure rating calculated from the listed hydrostatic design-stress.

**Table 28**

**SAFETY FACTORS VS. SERVICE FACTORS - PVC TYPE 1 THERMOPLASTIC PIPE**

PIPE CLASS	SERVICE FACTOR	HDS PSI	PRESSURE RATING PSI	SURGE PRESSURE AT 5 FT/SEC	MAXIMUM PRESSURE PSI	MAXIMUM STRESS PSI	SAFETY FACTOR
1-1/4" Sch. 80	0.5	2000	520	131.0	651.0	2503.5	3.38
1-1/4" Sch. 80	0.4	1600	416	131.0	547.0	2103.5	4.03

Pressure rating values are for PVC pipe, and for most sizes are calculated from the experimentally determined long-term strength of PVC extrusion compounds. Because molding compounds may differ in long term strength and elevated temperature properties from pipe compounds, piping systems

In each case, the hydrostatic design basis = 4000 psi, and the water velocity = 5 feet per second.

Comparing safety factor for this 1-1/4" Schedule 80 pipe at different service factors, it is instructive to note that changing from a service factor of 0.5 to a more conservative 0.4 increases the safety factor only by 16%.

$$100 \times \left( 1 - \frac{3.38}{4.03} \right) = 16\%$$

In the same way, changing the service factor from 0.4 to 0.35 increases the safety factor only by 9%. Changing the service factor from 0.5 to 0.35 increases the safety factor by 24%. From these comparisons it is obvious that little is to be gained in safety from surge pressures by fairly large changes in the hydrostatic design stress resulting from choice of more conservative service factors.

## FRICTION LOSS CHARACTERISTICS OF WATER THROUGH PLASTIC PIPE, FITTINGS AND VALVES

### INTRODUCTION

A major advantage of thermoplastic pipe is its exceptionally smooth inside surface area, which reduces friction loss compared to other materials.

Friction loss in plastic pipe remains constant over extended periods of time, in contrast to some other materials where the value of the Hazen and Williams C factor (constant for inside roughness) decreases with time. As a result, the flow capacity of thermoplastics is greater under fully turbulent flow conditions like those encountered in water service.

### C FACTORS

Tests made both with new pipe and pipe that had been in service revealed C factor values for plastic pipe between 160 and 165. Thus, the factor of 150 recommended for water in the equation below is on the conservative side. On the other hand, the C factor for metallic pipe varies from 65 to 125, depending upon age and interior roughening. The obvious benefit is that with plastic systems it is often possible to use a smaller diameter pipe and still obtain the same or even lower friction losses.

The most significant losses occur as a result of the length of pipe and fittings and depend on the following factors.

consisting of extruded pipe and molded fittings may have lower pressure ratings than those shown here, particularly at the higher temperatures. Caution should be exercised in design operating above 100°F.

1. Flow velocity of the fluid.
2. The type of fluid being transmitted, especially its viscosity.
3. Diameter of the pipe.
4. Surface roughness of interior of the pipe.
5. The length of the pipeline.

### Hazen and Williams Formula

The head losses resulting from various water flow rates in plastic piping may be calculated by means of the Hazen and Williams formula:

$$f = 0.2083 \left( \frac{100}{C} \right)^{1.852} \times \frac{q^{1.852}}{D_i^{4.8655}}$$

$$= .0983 \frac{q^{1.852}}{D_i^{4.8655}} \text{ for } C = 150$$

$$P = .4335f$$

### Where:

- f = Friction Head in ft. of Water per 100 ft of Pipe
- P = Pressure Loss in psi per 100 ft. of Pipe
- D<sub>i</sub> = Inside Diameter of Pipe, in.
- q = Flow Rate in U.S. gal/min
- C = Constant for Inside Roughness (C equals 150 thermoplastics)



# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## FLOW OF FLUIDS AND HEAD LOSS CALCULATIONS

Tables, flow charts, or a monograph may be used to assist in the design of a piping system depending upon the accuracy desired. In computing the internal pressure for a specified flow rate, changes in static head loss due to restrictions (valves, orifices, etc.) as well as flow head loss must be considered.

The formula in Table 29 can be used to determine the head loss due to flow if the fluid viscosity and density and flow rate are known. The head loss in feet of fluid is given by:

$$h = \frac{.186 fLV}{d^2}$$

f, the friction factor, is a function of the Reynolds number, a dimensionless parameter which indicates the degree of turbulence.

The Reynolds number is defined as:  $f = \frac{dVW}{12U}$

Figure 7 below shows the relationship between the friction factor, and the Reynolds number, R. It is seen that three distinct flow zones exist. In the laminar flow zone, from Reynolds numbers 0 to 2000, the friction factor is given by the equation:

$$f = \frac{64}{R}$$

Substituting this in the equation for the head loss, the formula for laminar flow becomes:

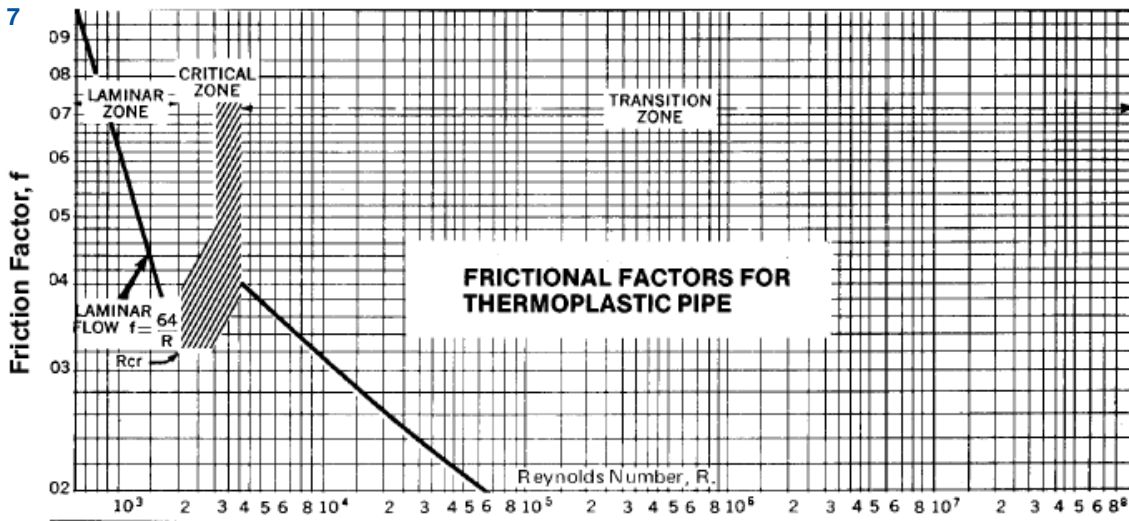
$$h = \frac{143 ULV}{Wd^2}$$

Flow in the critical zone, Reynolds numbers 2000 to 4000, is unstable and a surging type of flow exists. Pipe lines should be designed to avoid operation in the critical zone since head losses cannot be calculated accurately in this zone. In addition, the unstable flow results in pressure surges and water hammer which may be excessively high. In the transition zone, the degree of turbulence increases as the Reynolds number increases. However, due to the smooth inside surface of plastic pipe, complete turbulence rarely exists. Most pipe systems are designed to operate in the transition zone.

**TABLE 29**

FORMULAS FOR HEAD LOSS CALCULATIONS			
R=	SYMBOL	QUANTITY	UNITS
$R = \frac{dVw}{12u}$	B	flow rate	barrels/hour
$R = \frac{12u}{3160G}$	d	inside diameter	inches
$R = \frac{2220B}{kd}$	f	friction factor	dimensionless
$R = \frac{22,735Qw}{zd}$	G	flow rate	gallons/minute
	h	head loss	feet of fluid
When R = 4000:	k	kinematic viscosity	centistokes
$h = \frac{.186 fLV^2}{d}$	L	length of pipe	feet
$h = \frac{.0311 fLG^2}{d^5}$	P	pressure drop	lbs/in <sup>2</sup>
$P = \frac{fLB^2W}{9450d^2}$	Q	flow rate	ft <sup>3</sup> /sec.
$P = 43.5 \frac{fLQ^2W}{d^5}$	R	Reynolds number	dimensionless
	u	absolute viscosity	lb/ft-sec.
	V	velocity	ft./sec.
	w	density	lbs/ft <sup>3</sup>
	z	absolute viscosity	centipoises

**Fig. 7**



## MANNING EQUATION

The Manning roughness factor is another equation used to determine friction loss in hydraulic flow. Like the Hazen-Williams C factor, the Manning "n" factor is an empirical number that defines the interior wall smoothness of a pipe. PVC pipe has an "n" value that ranges from 0.008 to 0.012 from laboratory testing. Comparing with cast iron with a range of 0.011 to 0.015, PVC is at least 37.5 percent more efficient, or another way to express this would be to have equal flow with the PVC pipe size being one-third smaller than the cast iron. The following table gives the range of "n" value for various piping materials.

**TABLE 30**

PIPE MATERIAL	"n" RANGE
CAST IRON	0.011-0.015
WROUGHT IRON (BLACK)	0.012-0.015
WROUGHT IRON (GALVANIZED)	0.013-0.017
SMOOTH BRASS	0.009-0.013
GLASS	0.009-0.013
RIVETED AND SPIRAL STEEL	0.013-0.017
CLAY DRAINAGE TILE	0.011-0.017
CONCRETE	0.012-0.016
CONCRETE LINED	0.012-0.018
CONCRETE-RUBBLE SURFACE	0.017-0.030
PVC	0.008-0.012
WOOD	0.010-0.013

# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## COMPENSATING FOR THERMAL EXPANSION

Thermoplastics exhibit a relatively high coefficient of thermal expansion (see Relative Properties Chart page 13 and 14)—as much as ten times that of steel. When designing plastic piping systems, expansion of long runs must be considered. Installation temperature versus working temperature or summer to winter extremes must be considered.

One area where extreme temperature variations can occur is in a polypropylene drain application. Temperature in waste systems depends on quantity and temperature of the waste liquids discharged into the system. In general, the quantities of wastes discharged through waste systems from laboratories in educational institutions will be relatively small (a few gallons at a time), while industrial laboratories and processing systems may discharge large quantities of very hot or very cold water.

There are several methods of controlling or compensating for thermal expansion of piping systems: taking advantage of off-sets and change of direction in the piping and expansion joints.

1. Offsets—Most piping systems have occasional changes in direction which will allow the thermally induced length changes to be taken up in offsets of the pipe beyond the bends. Where this method is employed, the pipe must be able to float except at anchor points.
2. Expansion Joints—Expansion joints for pressure applications are generally expensive.

The expansion loops and offset tables as shown on following pages have been generated for elevated temperatures as noted beneath the table. If the change in temperature and working temperatures are lower than those used to derive expansion loop and offset tables, the figures will be conservative. These tables can be generated for any temperature and expansion by using the following equations and the modulus of elasticity and working stress at the given temperature.

Assume the pipe to be a cantilevered beam. Deflection of a cantilevered beam is  $\Delta L$

$$\Delta L = \frac{Pl^3}{3EI}$$

Where:

- P = Force Causing the Pipe to Deflect
- l = Length of Pipe that is Deflected, in.
- E = Modulus of Elasticity at System Temperature, psi
- I = Moment of Inertia
- e = Coefficient of Thermal Expansion, in./in. °F
- $\Delta T$  = Change of Temperature, °F
- $\Delta L$  = Change in Length =  $12e(\Delta T)$ , in.
- L = Length of Straight Pipe Run, ft.

Maximum stress equation:

$$S = \frac{Mc}{I}$$

Where:

- S = Working Stress at the System Temperature, psi
- M = Bending Moment, lb. ft. = Pl
- c = Pipe O.D./2, in.
- I = Moment of Inertia

By substituting in maximum stress equation:

$$S = \frac{Pl/D}{2I}$$

Rearranging:

$$P = \frac{2SI}{l/D}$$

Rearranging deflection equation:

$$P = \frac{3EI(\Delta L)}{l^3}$$

Equating both equations:

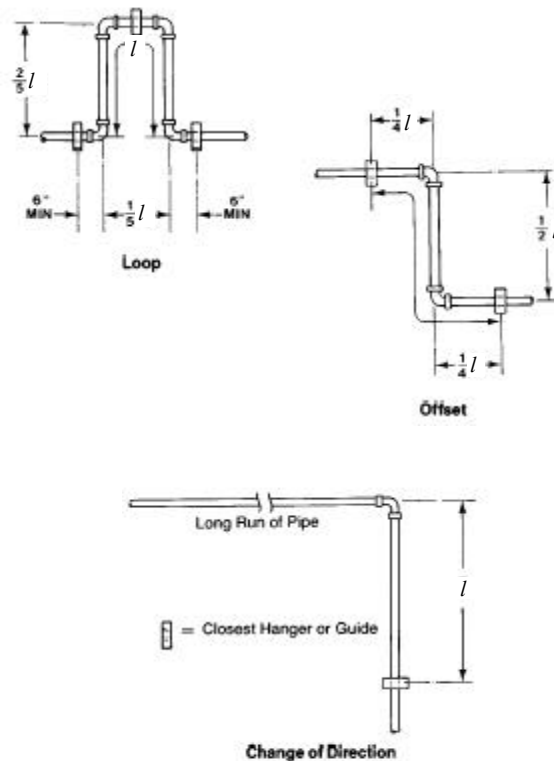
$$\frac{2SI}{l/D} = \frac{3EI(\Delta L)}{l^3}$$

Solving for loop length l:

$$l = \left( \frac{3ED(\Delta L)}{2S} \right)^{1/2}$$

**FIGURE 4**

Expansion Loop and Offset Configurations for Thermoplastics.



# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## THERMAL EXPANSION COMPENSATION

The change in length of Thermoplastic pipe with temperature variation should always be considered when installing pipe

lines and provisions made to compensate for this change in length. The following tables have been prepared to assist you in determining this expansion.

**TABLE 31 - THERMAL EXPANSION ΔL(in.) — PVC Type 1**

TEMP. CHANGE ΔT°F	LENGTH OF RUN IN FEET									
	10	20	30	40	50	60	70	80	90	100
30	.11	.22	.32	.43	.54	.65	.76	.86	.97	1.08
40	.14	.29	.43	.58	.72	.86	1.01	1.15	1.30	1.44
50	.18	.36	.54	.72	.90	1.08	1.26	1.40	1.62	1.80
60	.22	.43	.65	.86	1.08	1.30	1.51	1.73	1.94	2.16
70	.25	.50	.76	1.01	1.26	1.51	1.76	2.02	2.27	2.52
80	.29	.58	.86	1.15	1.44	1.73	2.02	2.30	2.59	2.88
90	.32	.65	.97	1.30	1.62	1.94	2.27	2.59	2.92	3.24
100	.36	.72	1.03	1.44	1.80	2.16	2.52	2.88	3.24	3.60

**Example:** Highest temperature expected— 120°F  
 Lowest temperature expected— 50°F  
 Total Change (ΔT) 70°F  
 Length of run—40 feet  
 From 70°F row on PVC chart read 1.01 in. length change (ΔL)  
 NOTE: Table is based on: ΔL = 12eL(ΔT)  
 Where: e = Coefficient of Thermal Expansion  
           = 3.0 × 10<sup>-6</sup> in./in.°F  
           L = Length of Run  
           ΔT = Temperature Change

**TABLE 32 - THERMAL EXPANSION ΔL(in.) — CPVC Schd. 80**

TEMP. CHANGE ΔT°F	LENGTH OF RUN IN FEET									
	10	20	30	40	50	60	70	80	90	100
20	.09	.18	.27	.36	.46	.55	.64	.73	.82	.91
30	.14	.27	.41	.55	.68	.82	.96	1.09	1.23	1.37
40	.18	.36	.55	.73	.91	1.09	1.28	1.46	1.64	1.82
50	.23	.46	.68	.91	1.14	1.37	1.60	1.82	2.05	2.28
60	.27	.55	.82	1.09	1.37	1.64	1.92	2.19	2.46	2.74
70	.32	.64	.96	1.28	1.60	1.92	2.23	2.55	2.87	3.19
80	.36	.73	1.09	1.46	1.82	2.19	2.55	2.92	3.28	3.65
90	.41	.82	1.23	1.64	2.05	2.46	2.87	3.28	3.69	4.10
100	.46	.91	1.37	1.82	2.28	2.74	3.19	3.65	4.10	4.56

**TABLE 33 - THERMAL EXPANSION ΔL(in.) — Copoly. Poly.**

TEMP. CHANGE ΔT°F	LENGTH OF RUN IN FEET									
	10	20	30	40	50	60	70	80	90	100
20	.15	.29	.44	.59	.73	.88	1.02	1.17	1.32	1.46
30	.22	.44	.66	.88	1.10	1.32	1.54	1.76	1.98	2.20
40	.29	.59	.88	1.17	1.46	1.76	2.05	2.34	2.64	2.93
50	.37	.73	1.10	1.46	1.83	2.20	2.56	2.93	3.29	3.66
60	.44	.88	1.32	1.76	2.20	2.64	3.07	3.51	3.95	4.39
70	.51	1.02	1.54	2.05	2.56	3.07	3.59	4.10	4.61	5.12
80	.59	1.17	1.76	2.34	2.93	3.51	4.10	4.68	5.27	5.86
90	.66	1.32	1.98	2.69	3.29	3.95	4.61	5.27	5.93	6.59
100	.73	1.46	2.20	2.93	3.66	4.39	5.12	5.86	6.59	7.32

**TABLE 34 - THERMAL EXPANSION ΔL(in.) — PVDF Schedule 80 and Pur-Flo**

TEMP. CHANGE ΔT°F	LENGTH OF RUN IN FEET									
	10	20	30	40	50	60	70	80	90	100
20	.19	.38	.58	.77	.96	1.15	1.34	1.54	1.73	1.92
40	.38	.77	1.15	1.54	1.92	2.30	2.69	3.07	3.46	3.84
50	.48	.96	1.44	1.92	2.40	2.88	3.36	3.84	4.32	4.80
60	.58	1.15	1.73	2.30	2.88	3.46	4.03	4.61	5.18	5.76
70	.67	1.34	2.02	2.69	3.36	4.03	4.70	5.38	6.05	6.72
80	.77	1.54	2.30	3.07	3.84	4.61	5.38	6.14	6.91	7.68
90	.86	1.73	2.59	3.46	4.32	5.18	6.05	6.91	7.78	8.64
100	.96	1.92	2.88	3.84	4.80	5.76	6.72	7.68	8.64	9.60

The following expansion loop and offset lengths have been calculated based on stress and modulus of elasticities at the temperature shown below each chart. To calculate the proper length of loop at other temperatures the following formula may be used:

$$l = \frac{\sqrt{3E(O.D.) \Delta L}}{2S}$$

Where:  
 ΔT = Temperature Change in °F  
 S = Thermal Stress, psi = e(ΔT)E  
 E = Modulus of Elasticity (found in relative properties chart on pages 482 and 483)  
 ΔL = Length Change in inches at ΔT (see tables above)  
 l = Total Length of Loop or Offset

**TABLE 35 - EXPANSION LOOPS AND OFFSET LENGTHS, PVC Type 1, Schedule 40 and 80**

NOM. PIPE SIZE	AVERAGE O.D.	LENGTH OF RUN IN FEET									
		10	20	30	40	50	60	70	80	90	100
		LENGTH OF LOOP "l" IN INCHES									
1/2	.840	11	15	19	22	24	27	29	31	32	34
3/4	1.050	12	17	21	24	27	30	32	34	36	38
1	1.315	14	19	23	27	30	33	36	38	41	43
1 1/4	1.660	15	22	26	30	34	37	40	43	46	48
1 1/2	1.900	16	23	28	33	36	40	43	46	49	51
2	2.375	18	26	32	36	41	45	48	52	55	58
3	3.500	22	31	38	44	49	54	58	63	66	70
4	4.500	25	35	43	50	56	61	66	71	75	79
6	6.625	30	43	53	61	68	74	80	86	91	96
8	8.625	35	49	60	69	78	85	92	98	104	110
10	10.750	39	55	67	77	87	95	102	110	116	122
12	12.750	42	60	73	84	94	103	112	119	126	133

NOTE: Table based on stress and modulus of elasticity at 130°F.  
 ΔT = 50°F  
 S = 600 psi  
 E = 3.1 × 10<sup>5</sup> psi



# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

**TABLE 36**  
EXPANSION LOOPS AND OFFSET LENGTHS, CPVC  
Schedule 80

NOM. PIPE SIZE	AVERAGE O.D.	LENGTH OF RUN IN FEET									
		10	20	30	40	50	60	70	80	90	100
		LENGTH OF LOOP "L" IN INCHES									
1/2	.840	15	21	26	30	33	37	39	42	45	47
3/4	1.050	17	22	27	31	34	38	40	43	46	48
1	1.315	19	26	32	37	42	46	49	53	56	59
1¼	1.660	21	30	36	42	47	52	56	59	63	67
1½	1.900	23	32	39	45	50	55	59	64	67	71
2	2.375	25	35	43	50	56	62	67	71	75	80
3	3.500	31	43	53	61	68	75	81	86	91	97
4	4.500	35	49	60	69	77	85	92	98	103	109
6	6.625	42	59	73	84	94	103	111	119	125	133
8	8.625	48	67	83	96	107	118	127	135	143	152
10	10.750	54	75	93	107	119	131	142	151	160	169
12	12.750	59	82	101	116	130	143	154	164	174	184

NOTE: Table based on stress and modulus of elasticity at 160°F.  
 $\Delta T = 100^\circ F$   
 $S = 750 \text{ psi}$   
 $E = 2.91 \times 10^5 \text{ psi}$

**TABLE 38**  
EXPANSION LOOPS AND OFFSET LENGTHS, PVDF  
Schedule 80

NOM. PIPE SIZE	AVERAGE O.D.	LENGTH OF RUN IN FEET									
		10	20	30	40	50	60	70	80	90	100
		LENGTH OF LOOP "L" IN INCHES									
1/2	.840	10	15	18	20	23	25	27	29	31	32
3/4	1.050	11	16	20	23	26	28	30	32	34	36
1	1.315	13	18	22	26	29	31	34	36	38	40
1¼	1.660	14	20	25	29	32	35	38	41	43	45
1½	1.900	15	22	27	31	34	38	41	44	46	49
2	2.375	17	24	30	34	38	42	46	49	52	54

NOTE: Table based on stress and modulus of elasticity at 180°F.  
 $\Delta T = 100^\circ F$   
 $S = 1060 \text{ psi}$   
 $E = 1.04 \times 10^5 \text{ psi}$

**TABLE 37**  
EXPANSION LOOPS AND OFFSET LENGTHS

COPOLYMER POLYPROPYLENE		LENGTH OF RUN IN FEET									
NOM. PIPE SIZE	AVERAGE O.D.	10	20	30	40	50	60	70	80	90	100
		LENGTH OF LOOP "L" IN INCHES									
1/2	.840	18	25	31	36	40	44	47	50	54	57
3/4	1.050	20	28	35	40	45	49	53	56	60	63
1	1.315	22	32	39	45	50	55	59	63	67	71
1¼	1.660	25	35	43	50	56	62	66	71	75	79
1½	1.900	27	38	46	54	60	66	71	76	81	85
2	2.375	30	42	52	60	67	74	79	85	90	95
3	3.500	36	52	63	73	81	89	96	103	109	115
4	4.500	41	58	71	83	92	101	109	117	124	131
6	6.625	50	71	87	100	112	123	132	142	151	159
8	8.625	57	81	99	114	128	140	151	162	172	181
10	10.750	64	90	111	128	143	156	169	181	192	202
12	12.750	69	98	121	139	155	170	184	197	209	220

NOTE: Table based on stress and modulus of elasticity at 160°F.  
 $\Delta T = 100^\circ F$   
 $S = 240 \text{ psi}$   
 $E = .83 \times 10^6 \text{ lb./in.}^2$

# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

These tables are based on:

$F = As =$  restraining force, lbs.

$A =$  Cross sectional wall area, in.<sup>2</sup>

$S = e(\Delta T)E$

$e =$  Coefficient of liner expansion\*

$E =$  Modulus of elasticity\*

$\Delta T =$  Temperature change, °F

\*All values are available from relative properties chart on pages 482 and 483

**TABLE 39**

**RESTRAINT FORCE "F" (LB.)—PVC Type 1  
Schedule 40 and 80.**

PIPE SIZE	SCHEDULE 40 PVC			SCHEDULE 80 PVC		
	CROSS SECTIONAL WALL AREA (IN <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$	$\Delta T = 100^\circ\text{F}$	CROSS SECTIONAL WALL AREA (IN <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$	$\Delta T = 100^\circ\text{F}$
		S = 630 PSI	S = 1260 PSI		S = 630 PSI	S = 1260 PSI
1/2	.250	155	310	.320	200	400
3/4	.333	210	420	.434	275	550
1	.494	310	620	.639	405	810
1¼	.669	420	840	.882	555	1,110
1½	.800	505	1,010	1.068	675	1,350
2	1.075	675	1,350	1.477	930	1,860
3	2.229	1,405	2,810	3.016	1,900	3,800
4	3.174	2,000	4,000	4.407	2,775	5,550
6	5.581	3,515	7,030	8.405	5,295	10,590
8	8.399	5,290	10,580	12.763	8,040	16,080
10	11.908	7,500	15,000	18.922	11,920	23,840
12	15.745	9,920	19,840	26.035	16,400	32,800

**TABLE 40**

**RESTRAINT FORCE "F" (LB.), CPVC Schedule 80**

PIPE SIZE	CROSS SECTIONAL WALL AREA (IN. <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$ S = 805 PSI	$\Delta T = 100^\circ\text{F}$ S = 1610 PSI
1/2	.320	260	520
3/4	.434	350	700
1	.639	515	1,030
1¼	.882	710	1,420
1½	1.068	860	1,720
2	1.477	1,190	2,380
3	3.016	2,430	4,860
4	4.407	3,550	7,100
6	8.405	6,765	13,530
8	12.763	10,275	20,550
10	18.922	15,230	30,460
12	26.035	20,960	41,920

**TABLE 41**

**RESTRAINT FORCE "F" (LB.), Copolymer Polypropylene  
Schedule 80**

PIPE SIZE	CROSS SECTIONAL WALL AREA (IN. <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$ S = 550 PSI	$\Delta T = 100^\circ\text{F}$ S = 1110 PSI
1/2	.320	147	294
3/4	.434	199	398
1	.639	293	586
1¼	.882	404	808
1½	1.068	489	978
2	1.477	663	1,325
3	3.016	1,381	2,762
4	4.407	2,018	4,036
6	8.405	3,899	7,698
8	12.763	5,895	11,690
10	18.922	8,666	17,332
12	26.035	11,929	23,848

**TABLE 42**

**RESTRAINT FORCE "F" (LB.), PVDF Schedule 80**

PIPE SIZE	CROSS SECTIONAL WALL AREA (IN. <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$ S = 850 PSI	$\Delta T = 100^\circ\text{F}$ S = 1700 PSI
1/2	.320	270	540
3/4	.434	370	740
1	.639	540	1,080
1¼	.882	750	1,500
1½	1.068	905	1,810
2	1.477	1,255	2,510
3	3.016	2,565	5,130
4	4.407	3,745	7,490

**TABLE 43**

**RESTRAINT FORCE "F" (LB.), PVDF**

PIPE SIZE	CROSS SECTIONAL WALL AREA (IN. <sup>2</sup> )	$\Delta T = 50^\circ\text{F}$ S = 850 PSI	$\Delta T = 100^\circ\text{F}$ S = 1700 PSI
¼	0.167	142	284
⅜	0.213	180	360
1	0.346	294	588
1½	0.681	579	1158
2	0.876	745	1490
3	1.791	1522	3044
4	2.706	2300	4600